# Main-Group Catalysis for H<sub>2</sub> Purification Based on Liquid Organic Hydrogen Carriers

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#### Abstract

We demonstrate a strategy to separate  $H_2$  from a gaseous mixture of  $H_2/CO/CO_2/CH_4$  that can include an excess of CO and CO<sub>2</sub> relative to  $H_2$  and simultaneously store it in *N*-heterocyclic compounds that act as liquid organic hydrogen carriers (LOHCs), which can be applied to produce  $H_2$  by subsequent dehydrogenation. Our results demonstrate that LOHCs can potentially be used for  $H_2$  purification from CO- and CO<sub>2</sub>-rich crude  $H_2$  in addition to their well-established use in  $H_2$  storage.

## **1. Introduction**

Molecular hydrogen (H<sub>2</sub>) is an essential reductant and one of the most promising energy carriers of the future. Thus, it can be expected that a huge amount of H<sub>2</sub>, on a magnitude of more than  $10^{12}$  standard cubic feet/year, will be produced from a wide range of hydrocarbon and renewable resources.<sup>1</sup> The predominant contemporary route to H<sub>2</sub> production includes the intensive purification of crude H<sub>2</sub>, which is a gaseous mixture of H<sub>2</sub>, CO, CO<sub>2</sub>, and other components that is produced by gasification, reforming, and/or water-gas shift (WGS) (process I in Fig. 1). Purification processes such as pressure swing adsorption (PSA), membrane separation, and cryogenic separation critically determine the purity of the H<sub>2</sub> and influence the total energy consumption of the H<sub>2</sub> production process, making it cost-inefficient. Thus, although H<sub>2</sub> can currently be stored after or during the process I in Fig.

1, we envisaged a solution where H<sub>2</sub> could be stored in its carrier directly from crude  $H_2$ . which often includes more CO than  $H_2$ , without the requirement for any of the aforementioned purification shift and processes (process II in Fig. 1).<sup>3</sup> Moreover, the recovery of H<sub>2</sub> after our proposed path ultimately leads to the production of highly pure H<sub>2</sub>.

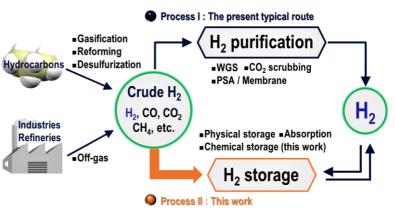


Fig. 1 Research background and concept of this work.

# 2. Experiment

A 30 mL autoclave was charged with 2-methylquinoline and triarylborane. Once sealed, the

autoclave was pressurized with  $H_2/CO/CO_2$  (4 atm each) and heated to 100 °C for 2 h. After cooling to room temperature, all volatiles were removed *in vacuo*. Then, the reaction mixture was transferred into a 10 mL two-neck flask. The reaction mixture was then stirred at 200 °C for 3 h.

## **3. Results and discussion**

In the presence of catalytic amount of our original triarylborane catalyst, the hydrogenation of 2-methylquinoline proceeded effectively (upto 1520 turnover) at 100 °C under the solvent-free, mixed-gas (H<sub>2</sub>/CO/CO<sub>2</sub>; 1/1/1 molar) conditions (Fig. 2). After degasification to remove CO and CO<sub>2</sub>, dehydrogenation from the tetrahydroquinoline was carried out at 200 °C, which afforded H<sub>2</sub> of >99.9% purity with the regeneration of 2-methylquinoline.

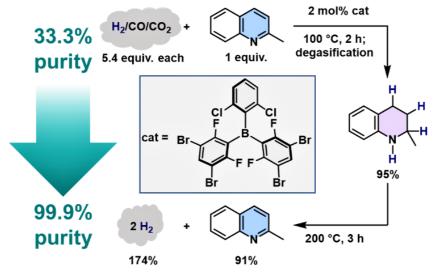


Fig. 2  $H_2$  purification based on the borane-catalyzed hydrogenation of 2-methylquinoline under mixed-gas conditions and subsequent catalytic dehydrogenation.

## 4. Conclusions

The present results demonstrate a proof-of-concept for a H<sub>2</sub>-purification technology based on LOHCs that goes beyond their well-established use in H<sub>2</sub> storage. This technology can be expected to change the industrial value of crude H<sub>2</sub> containing substantial amounts of CO, CO<sub>2</sub>, and CH<sub>4</sub>, which can be produced from a variety of carbon resources such as biomass and industrial off-gases. Moreover, this work demonstrates a new aspect of main-group catalysis beyond its application as a simple alternative to well-established transition-metal-catalyzed processes, i.e., the main-group-catalyzed hydrogenation of unsaturated molecules under mixed-gas conditions.

# References

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